

# Adsorption capability of activated carbon synthesized from coconut shell

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## Abstract

Activated carbon was synthesized from coconut shells. The Brunauer, Emmett and Teller surface area of the synthesized activated carbon was found to be 1640 m<sup>2</sup>/g with a pore volume of 1.032 cm<sup>3</sup>/g. The average pore diameter of the activated carbon was found to be 2.52 nm. By applying the size-strain plot method to the X-ray diffraction data, the crystallite size and the crystal strain was determined to be 42.46 nm and 0.000489897, respectively, which indicate a perfect crystallite structure. The field emission scanning electron microscopy image showed the presence of well-developed pores on the surface of the activated carbon. The presence of important functional groups was shown by the Fourier transform infrared spectroscopy spectrum. The adsorption of methyl orange onto the activated carbon reached 100% after 12 min. Kinetic analysis indicated that the adsorption of methyl orange solution by the activated carbon followed a pseudo-second-order kinetic mechanism ( $R^2 > 0.995$ ). Therefore, the results show that the produced activated carbon can be used as a proper adsorbent for dye containing effluents.

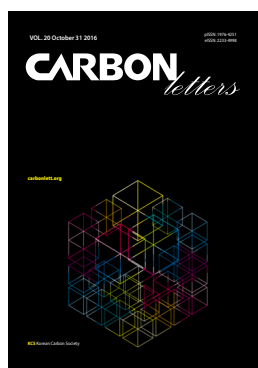
**Key words:** coconut shell, activated carbon, dye adsorption, size-strain plot, specific surface area

## 1. Introduction

In this era of industrialization, industries like textile (especially in the dyeing sector), leather, carpet, rubber, food processing, pharmaceutical, cosmetic, plastic, pulp and paper manufacturing use synthetic dyes regularly and discharge a large amount of dye containing water into the environment [1-4]. Nowadays, the annual production of commercial dyes is over 9 million tons with over one hundred thousand types of dyes [5,6]. It has been reported that about 10%–20% of dyes are discharged into water during the dyeing process [7]. Dyes usually contain recalcitrant molecules which are potentially carcinogenic, toxic and resistant to aerobic digestion and inhibit the reaction of oxidizing agents [8,9]. The very complex molecular structures of these dyes make them imperishable [10,11]. Even a small amount of dye can be harmful to both terrestrial and aquatic animals as well as humans [12]. Thus, these dyes require proper treatment before being discharged into the environment.

Among the physical, chemical and biological methods of dye removal, oxidation (using oxidizing agents like ozone, ultraviolet [UV] irradiation, and hydrogen peroxide), membrane separation, coagulation and flocculation, and adsorption are commonly used [3,13]. However, other than the adsorption techniques, these methods have either high costs and/or are technically complicated [14]. The adsorption method is highly preferable due to its low cost consumption, easy operation, higher efficiency, insensitivity to toxic materials and versatility [1,13,15-17].

The commonly used adsorbents are modified clays, waste materials, natural polymers and biopolymers (usually poly saccharides such as chitosan and its derivatives), zeolites,



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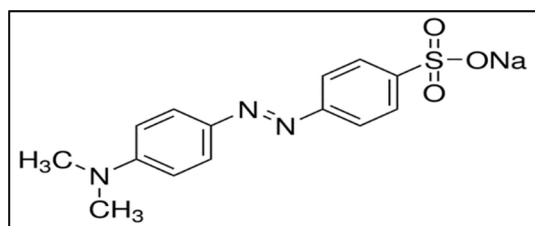


Fig. 1. Chemical structure of methyl orange.

activated carbon, etc. Other than activated carbon, the other adsorbents have some undesirable disadvantages in dye removal such as complex separation techniques from the adsorbate, little or no resistance against acid solutions, and poor mechanical strength and versatility. Additionally, these adsorbents need a long contact time with the adsorbate [18-22]. Therefore, with a high specific surface area, large pore volume, suitable pore size (2–50 nm), high degree of surface reactivity and effective adsorption quality, activated carbon has become the most desirable adsorbent [23-26].

Methyl orange is one of the most used anionic dyes, which belongs to the azo group of dyes, in textile manufacturing and paper and food processing industries. The presence of the azo group ( $-N=N-$ ) in the molecules of methyl orange and its low biodegradability make it a serious threat to the environment [27]. The chemical structure of methyl orange is shown in Fig. 1.

Many studies have been done on the removal of dye molecules from aqueous solutions by activated carbon; however, most of them were unable to remove dye molecules completely (100%) in a short time period [28-32]. Hesas et al. [28] reported the highest adsorption (94.6%) among all the studies. The reason for this could be due to the relatively smaller surface area of activated carbon because it is obvious that a higher surface area leads to a higher adsorption efficiency [33]. Therefore, the aim of this study was to synthesize activated carbon from coconut shells with a higher surface area to completely remove dye molecules from an aqueous solution within the shortest possible time.

In this study, activated carbon was synthesized from a coconut shell and then characterized. Additionally, the synthesized activated carbon in this study was verified as an effective adsorbent by the removal of methyl orange (sodium 4-[(4-dimethylamino) phenyldiazenyl] benzene sulfonate).

## 2. Experimental

### 2.1. Synthesis of the activated carbon

In this study, we used coconut shells to produce activated carbon and methyl orange for the adsorption test. The use of both were in compliance with the ethical standards of Malaysian government. A coconut shell was washed with distilled water to remove undesirable impurities and dried in an oven at 120°C for 24 h. The washed and dried coconut shell was carbonized at 450°C for 3 h at a heating rate of 10°C/min. under a flow of purified nitrogen. The carbonized sample was washed with distilled water and kept in an oven at 70°C for 48 h for complete drying. The dried char was mixed with potassium hydroxide (KOH) pellets

in a 1:4 (KOH/char) impregnation ratio followed by the addition of 15 mL of distilled water to the mixture. Then, the mixture was stirred with a magnetic stirrer for 4 h. The activation step was done in a tube furnace at 400°C for 30 min and 600°C for 2 h with a heating rate of 5°C/min. under a purified nitrogen flow. The activated product was washed with deionized water and hydrochloric acid until the pH of the washing solution reached 6–7. Then, the activated carbon was kept in an oven for 24 h.

### 2.2. Characterization of the activated carbon

Synthesized activated carbon was analyzed with the  $N_2$  adsorption desorption test based on the Brunauer-Emmett-Teller (BET) principle, X-ray diffraction (XRD), field emission scanning electron microscopy (FESEM) and Fourier transform infrared spectroscopy (FTIR).

#### 2.2.1. Nitrogen adsorption isotherm analysis

The pore structure characteristics of the activated carbon were determined by nitrogen adsorption with a Sorptomatic 1990. During the experiment, the carbon was degassed at 120°C for 12 h in a vacuum condition. The BET surface area was determined with the standard BET equation applied in a relative pressure range from 0.06 to 0.3. The total pore volume was calculated at a relative pressure of approximately 0.985, and at this relative pressure, all pores were completely filled with nitrogen gas.

#### 2.2.2. Crystallographic analysis

Powder XRD patterns were recorded using the PANalytical Empyrean X-ray diffractometer (EA Almelo, the Netherlands) with monochromated Cu K $\alpha$  radiation ( $\lambda = 1.54056 \text{ \AA}$ ) operated at 45 kV and 40 mA with a step size of 0.026° and a scanning rate of 0.1° s<sup>-1</sup> over a 2 $\theta$  range from 5° to 80°. The crystallite size of the produced sample was calculated with the following size-strain plot (SSP) equation [34].

$$(d_{hkl}\beta_{hkl}\cos\theta)^2 = \frac{K}{D}(d_{hkl}^2\beta_{hkl}\cos\theta) + \left(\frac{\varepsilon}{2}\right)^2 \quad (1)$$

Here,  $d_{hkl}$  represents the lattice distance between the ( $hkl$ ) planes;  $\beta_{hkl}$  is the peak full width at half height (FWHM) in radians. K, D,  $\varepsilon$  and  $\theta$  correspond to the constant ( $\frac{4}{3}$ ), crystallite size, lattice strain and half diffraction angle (radian). When  $(d_{hkl}\beta_{hkl}\cos\theta)^2$  is plotted against  $(d_{hkl}^2\beta_{hkl}\cos\theta)$  for the characteristics peaks of the activated carbon, the crystallite size is measured from the slope of the linearly fitted data and the strain from the root of the y-intercept.

#### 2.2.3. Surface morphology analysis

FESEM (high-resolution FEI Quanta 200F; Hitachi, Tokyo, Japan) was used to observe the surface morphology of the activated carbon, and energy dispersive X-ray spectroscopy (EDS) analysis was done to determine the elements in the sample. The average composition was obtained by taking the average of 4 points.

#### 2.2.4. FTIR analysis

Nicolet iS10 FTIR spectrometer from Thermo Scientific with a spectral range from 4000 to 400 cm<sup>-1</sup> was used to determine the functional groups of the activated carbon.

## 2.3. Adsorption test

In the adsorption test, 0.2 g of activated carbon were added to 0.02 L of methyl orange solution (30 mg/L) and agitated gently with a magnetic stirrer for 12 min to examine the adsorption behavior of the activated carbon. The sample was collected at different time intervals, and the dye concentration ( $C_t$ ) was calculated with the Varian CARY 50 probe type UV-vis spectrophotometer (Agilent Technologies Inc., Santa Clara, CA, USA). The amount of dye adsorbed ( $q_t$ ) onto the activated carbon was calculated with the following formula [35,36]:

$$q_t = \frac{c_0 - c_t}{m} V \quad (2)$$

here,  $C_0$  and  $C_t$  represent, respectively, the initial and equilibrium concentrations of methyl orange solution in ( $\text{mg L}^{-1}$ ), and  $V$  is the volume of the solution in liters, and  $m$  is the weight of the activated carbon used in grams.

The percentage removal of methyl orange was calculated with the following equation [37]:

$$\text{Removal}(\%) = \frac{c_0 - c_t}{c_0} \times 100 \quad (3)$$

## 3. Results and Discussion

### 3.1. Nitrogen adsorption-desorption isotherm of the synthesized activated carbon

The adsorption capacity of an adsorbent largely depends on the number of pores and the size of the surface area. Porosity in carbon is developed through an activation process by creating a more orderly porous structure [38]. There are usually four stages in pore development during the activation process: 1) opening of previously inaccessible pores; 2) creation of new pores by selective activation; 3) widening of existing pores; and 4) merging of existing pores due to pore wall breakage [39]. Fig. 2 shows the nitrogen adsorption-desorption isotherm of the activated carbon prepared by KOH activation.

Fig. 2a shows that the adsorption-desorption isotherm of the activated carbon is for a Type IV isotherm based on the Interna-

tional Union of Pure and Applied Chemistry (IUPAC) classification [40]. A characteristic feature of Type IV isotherms is that they possess a hysteresis loop which is associated with capillary condensation taking place in the mesopores which limits uptake at high relative pressures. From Fig. 2b, it is clear that the pore size ranges between 2 and 20 nm which proves the mesoporosity of the particle. The average pore diameter can be calculated with the following equation [41]:

$$D = \frac{4V}{A} \quad (4)$$

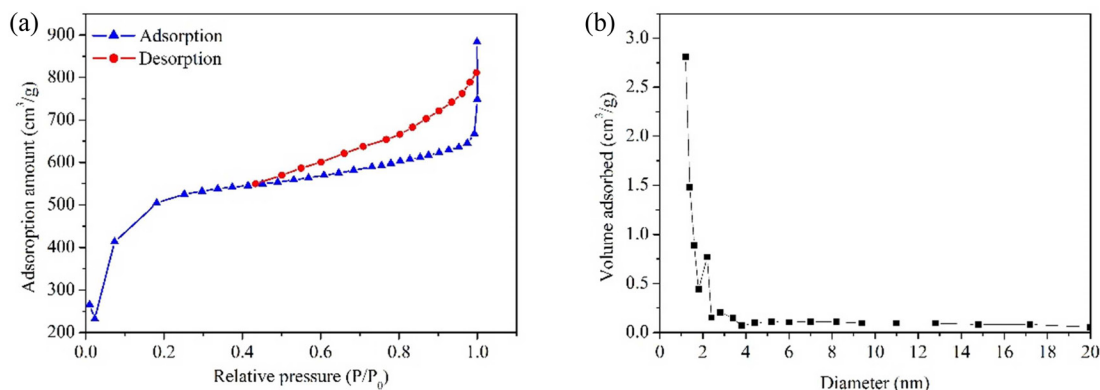
here,  $V$  and  $A$  denote the pore volume and specific surface area measured by the BET method. Therefore, the specific surface area and pore volume of the activated carbon were found to be  $1640 \text{ m}^2/\text{g}$  and  $1.032 \text{ cm}^3/\text{g}$ , respectively. The average pore diameter was found to be 2.52 nm.

### 3.2. Crystallographic analysis of the activated carbon

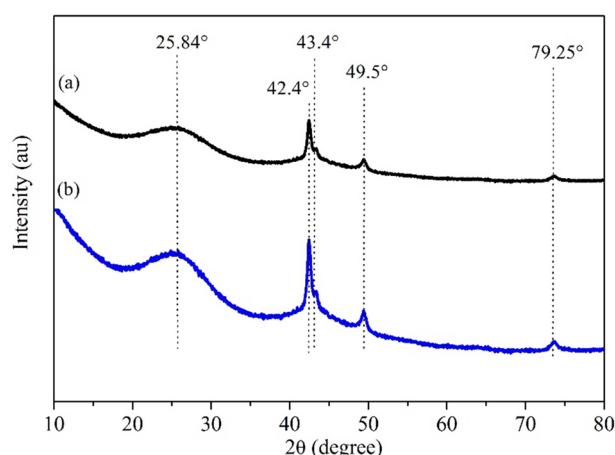
The synthesized activated carbon can be crystallographically characterized with XRD. Fig. 3 shows the X-ray diffractograms of the activated carbon before and after the activation process. Fig. 3a shows that the carbonized sample has five major peaks at  $25.84^\circ$ ,  $42.4^\circ$ ,  $43.4^\circ$ ,  $49.5^\circ$ , and  $79.25^\circ$  ( $2\theta$ ). These peaks are also found in the final activated carbon sample.

The amorphous peak detected at around  $26^\circ$  ( $2\theta$ ) is assigned to the reflection from the (002) plane. The peaks at  $42^\circ$  and  $79^\circ$  ( $2\theta$ ) are assigned to the overlapped reflection from the (100), (101) and (110) plane, respectively [42]. The diffraction peaks at  $2\theta = 26$  and  $42$  signify that both samples are composed of a carbonaceous material [43].

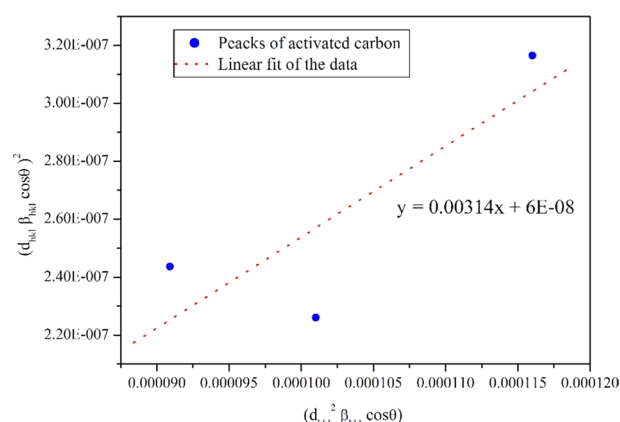
Peaks corresponding to potassium metal and potassium oxides usually appear at  $42^\circ$  and  $49^\circ$  ( $2\theta$ ) with  $42^\circ$  ( $2\theta$ ) denoting the "K" metal and  $49^\circ$  ( $2\theta$ ) the  $\text{K}_2\text{CO}_3$  compound. The intensity of these peaks is increased in the sample after the activation process (Fig. 3b) compared to the sample before activation (Fig. 3a). The reason for this may be due to the overlapping of the peaks for K with the peaks for the (100), (101) plane of carbonaceous materials. A gasification reaction occurred during the KOH activation process in which KOH was converted to either K metal or  $\text{K}_2\text{CO}_3$  [44]. Potassium metal remains in the final



**Fig. 2.** (a)  $\text{N}_2$  adsorption-desorption isotherms and (b) pore size distribution curve based on the Brunauer-Emmett-Teller method for the activated carbon.



**Fig. 3.** X-ray diffraction patterns (a) carbonized sample and (b) activated carbon sample.

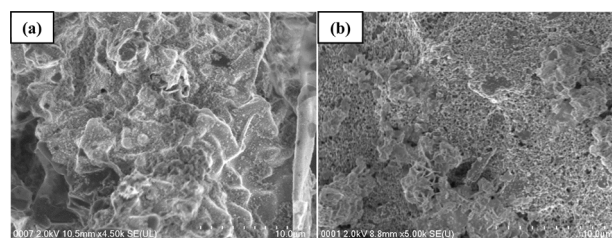


**Fig. 4.** The size-strain plot of the activated carbon.

activated carbon because the boiling point of K is 780°C [45]. However, 600°C was the highest temperature used during the activation process in this study.

The presence of the (100) and (110) plane indicates that the produced activated carbon is composed of small domains of ordered graphene sheets which shows the regularity of the crystal structure [46]. Liu and Watanasiri [47] calculated the theoretical (002) Bragg peaks for powder samples to determine whether the sample is made of randomly oriented single layers, bilayers and trilayers as well as mixtures of randomly oriented bilayers. And according to Liu's result, synthesized activated carbon consists of randomly oriented single and multi-layer domains.

The FWHM of the four crystalline peaks at 42.3916°, 43.4253°, 49.4610° and 79.2510° (2θ) found in the activated carbon sample (Fig. 3b) were used to calculate the crystallite size of the activated carbon. By applying the SSP method to the XRD data (as described in section 2.2.2), the crystallite size (D) was found to be 42.46 nm, and the corresponding crystal strain (ε) was equal to 0.000489897. The SSP is shown in Fig. 4. The crystallite size and crystal strain values show that the synthesized activated carbon has a perfect crystalline structure with no lattice displacement.



**Fig. 5.** Field emission scanning electron microscopy micrographs of the activated carbon (a) before activation and (b) after activation.

**Table 1.** Composition of the activated carbon

	Carbon (C) (%)	Oxygen (O) (%)	Nitrogen (N) (%)	Silicone (Si) (%)
Spot 1	76.7	20.5	2.6	0.2
Spot 2	78.9	18.5	2.3	0.3
Spot 3	79.1	17.9	2.8	0.2
Spot 4	83.5	13.6	2.7	0.2
Average	79.55	17.625	2.6	0.225

### 3.3. Surface morphology of the activated carbon

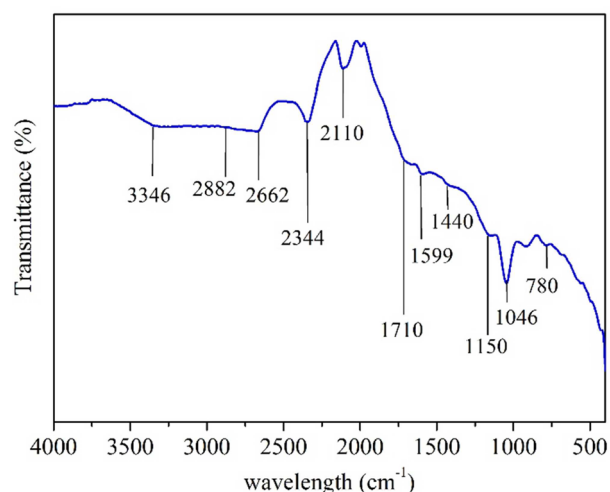
Fig. 5 shows the microstructure of the activated carbon before and after the activation process. It can be seen from Fig. 5a that before the carbonization process, a much smaller number of pores was present on the external surface of the activated carbon. However, after the activation process, well-developed pores are clearly visible on the surface of the activated carbon. This is in agreement with the 1.032 cm<sup>3</sup>/g pore volume found by the BET surface analysis. These pores might be due to the evaporation of the chemical reagent (KOH) used during the carbonization process leaving behind the porous surface of the activated carbon [38].

The average compositions of the activated carbon are summarized in Table 1 which were acquired by the EDS analysis. Of note is that the activated carbon sample has a high carbon content. The presence of oxygen is mainly due to inadequate washing of the material. The presence of nitrogen may be due to the nitrogen gas flow during the carbonization and activation process. And the very low amount of silicone indicates the presence of a small amount of impurities. Thus, it can be concluded that carbon is the predominant component in the sample which indicates the carbonaceous nature of the sample.

### 3.4. FTIR analysis

The FTIR spectrum of the activated carbon is shown in Fig. 6. The broad band at 3346 cm<sup>-1</sup> is related to the valence vibration of the hydrogen bonded O-H groups [48]. The reason for the occurrence of this band can be assigned to the O-H stretching mode of the hexagonal groups and adsorbed water. Additionally, the presence of strong hydrogen bonds is indicated by the

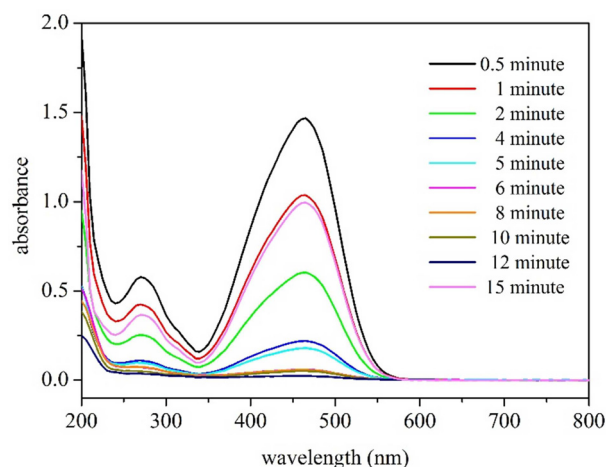




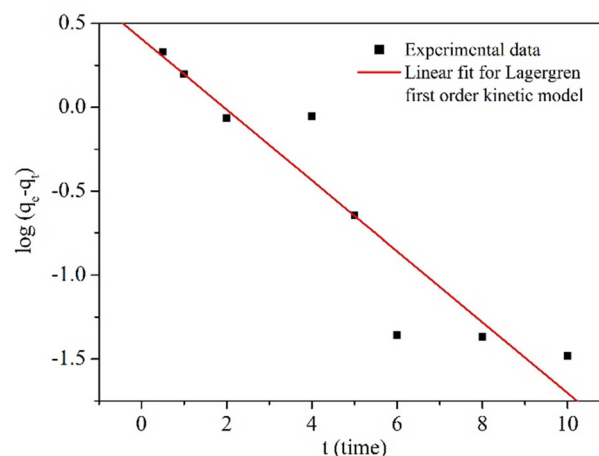
**Fig. 6.** Fourier transform infrared spectroscopy spectrum of the activated carbon synthesized from a coconut shell.

position and asymmetry of this band at lower wave numbers [49]. The shoulder band at 2882  $\text{cm}^{-1}$  may originate from the C-H stretching in the  $(-\text{CH}_2)$  and  $(-\text{CH}_3)$  groups [50,51]. The relatively wide band at 2344  $\text{cm}^{-1}$  may either correspond to the symmetric  $(\text{NH}_3^+)$  stretching frequency [52] or to the carbon-oxygen bonds in the ketene groups [50]. Another relatively broad peak at  $\sim 2100 \text{ cm}^{-1}$  is attributed to the allene ( $\text{C}=\text{C}=\text{C}$ ) group [53]. A very small peak near 1700  $\text{cm}^{-1}$  is assigned to the  $\text{C}=\text{O}$  stretching vibrations of ketones, aldehydes, lactones or carboxyl groups. The weak intensity of this peak indicates that this sample contains a small amount of carboxyl groups [53]. The band at 1599  $\text{cm}^{-1}$  indicates the presence of  $(\text{C}-\text{H})$ ,  $(-\text{C}=\text{C}-)$  and aromatic  $\text{C}=\text{C}$  groups [54]. Moreover, the band at 1440  $\text{cm}^{-1}$  may correspond to the O-H bending band. In the region (1400–1600)  $\text{cm}^{-1}$ , there are clusters of complex bands, which may be due to the presence of aromatic ( $\text{C}=\text{C}$ ) bands and various substitution modes of the aromatic rings [55]. The broad band at 1150  $\text{cm}^{-1}$  has been assigned to C-O single bonds such as those in ethers, phenols, acids and esters [50,51].

The sharp peak at 1046  $\text{cm}^{-1}$  represents the alcoholic C-O stretching vibration [55]. Bands below 950  $\text{cm}^{-1}$  correspond to the out-of-plane deformation vibrations of the C-H groups in the aromatic structure [49,56]. In this region, the bands at 590  $\text{cm}^{-1}$  and 675  $\text{cm}^{-1}$  generally correspond to the stretch of the S=O and S-O group, and 670  $\text{cm}^{-1}$  represents physisorbed carbon dioxide [57]. Other peaks detected in this region at 780  $\text{cm}^{-1}$ , 652  $\text{cm}^{-1}$  and 608  $\text{cm}^{-1}$ , respectively, are assigned to the C-H out-of-plane bending in benzene derivatives, O-H stretching and C-O-H twist. The C-H out-of-plane bending in benzene derivatives has been commonly found on the surface of various activated carbons [58,59]. There are no peaks for  $\text{SiO}_2$  at 1101, 944 and 470  $\text{cm}^{-1}$ , which indicate that the synthesized activated carbon consists of no or very few  $\text{SiO}_2$  [60]. This result is also shown by the EDS analysis in this study. Additionally, the FTIR spectra found here are in accordance with the results reported by Jung et al. [61] on a commercial granular activated carbon.



**Fig. 7.** Ultraviolet visible spectra of the methyl orange solution with different contact times with the activated carbon.



**Fig. 8.** Linear regression of the Lagergren first order kinetic model for the adsorption of methyl orange at room temperature.

### 3.5. Adsorption of methyl orange by the synthesized activated carbon

The UV-vis spectra of methyl orange solution in contact with activated carbon is shown in Fig. 7. It can be seen from Fig. 7 that the characteristic peaks of benzene and the azo linkage of the methyl orange were found in the initial UV-vis spectra of the methyl orange at a wavelength of 270 and 464.9 nm, respectively. Therefore, it was observed that the intensity was reduced with an increase in the contact time. After 12 min, methyl orange removal reached 100%.

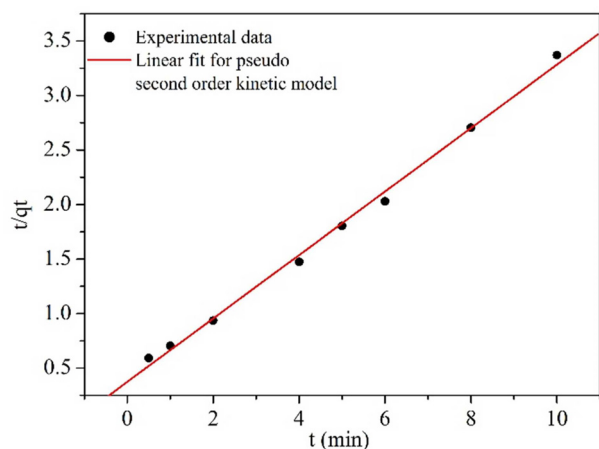
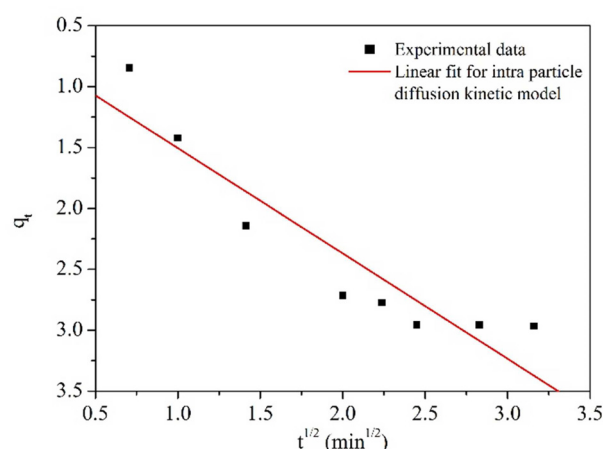
In order to predict the adsorption behavior of the activated carbon, Lagergren-first-order [62], pseudo-second-order [63] and Weber and Morris intra-particle diffusion reaction models [64] were used to determine the kinetics of the adsorption of methyl orange from an aqueous solution.

Lagergren first order kinetic model; the linear form of the Lagergren first order kinetic model is represented by the following formula.

**Table 2.** Kinetic parameters for the adsorption of methyl orange on the activated carbon

Kinetic model	Concentration (mg L <sup>-1</sup> )	q <sub>e</sub> (exp., mg g <sup>-1</sup> )	q <sub>e</sub> (cal., mg g <sup>-1</sup> )	Rate constant	R <sup>2</sup>	SD (%)	C (mg g <sup>-1</sup> )
Lagergren first order kinetic model			2.56	0.486 min <sup>-1</sup>	0.8868	27.493	NA
Pseudo second order kinetic model	30	3	3.14	0.2266 g mg <sup>-1</sup> min <sup>-1</sup>	0.9959	6.768	NA
Intra particle diffusion kinetic model			NA	0.86 mg g <sup>-1</sup> min <sup>-1</sup>	0.8632	32.361	0.63952

q<sub>e</sub>, equilibrium adsorption capacity ; SD, standard deviation.

**Fig. 9.** Linear regression of the pseudo second order kinetic model for the adsorption of methyl orange at room temperature.**Fig. 10.** Linear regression of the intra particle diffusion kinetic model for the adsorption of methyl orange at room temperature.

$$\log(q_e - q_t) = \log q_e - \frac{k_1 t}{2.303} \quad (5)$$

, where  $q_e$  and  $q_t$  represent the amounts of methyl orange adsorbed (mg/g) at equilibrium and at time  $t$ , respectively.  $k_1$  (min<sup>-1</sup>) is the Lagergren rate constant. Fig. 8 shows the plots of  $\log(q_e - q_t)$  versus  $t$  of the Lagergren first order kinetic model. Values for  $q_e$  and  $k_1$  at different initial concentrations were calculated, respectively, from the slope and intercept. These are presented in Table 2.

The pseudo-second-order kinetic model; the linear form of the pseudo-second-order kinetic model is represented by the following formula.

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (6)$$

, where  $q_e$  and  $q_t$  represent the amounts of methyl orange adsorbed (mg/g) at equilibrium and at time  $t$ , respectively. The rate constant of the pseudo second order adsorption model is represented by  $K_2$  in (g/mg/min.). Fig. 9 shows the plots of  $t/q_t$  versus  $t$ . Values for  $K_2$  and  $q_e$  were calculated, respectively, from the slope and intercept point of the graph. These values are presented in Table 2.

Weber and Morris intra-particle diffusion reaction model; the linear form of the intra-particle diffusion reaction model is represented by the following formula.

$$q_t = k_{id} t^{1/2} + c \quad (7)$$

, where  $c$  is the intercept which reflects the boundary layer effect;  $q_e$  and  $q_t$  represent the amounts of methyl orange adsorbed (mg/g) at equilibrium and at time  $t$ , respectively, and  $k_{id}$  is the intra particle diffusion reaction model. Fig. 10 shows the plot of  $q_t$  versus  $t^{1/2}$ . The values for  $K_{id}$  and  $c$  were calculated, respectively, from the slope and intercept and are presented in Table 2.

Of note in Table 2 is that there is a notable difference between the theoretical value of  $q_e$  (2.56 mg g<sup>-1</sup>) determined from the Lagergren first order kinetic model and the experimental value. Moreover, the correlation coefficient ( $R^2 = 0.7201$ ) is significantly low. Therefore, the adsorption kinetics of methyl orange cannot be explained by this model. On the other hand, it is obvious from Table 2 that the adsorption kinetics of methyl orange on the activated carbon can be better interpreted by the pseudo-second-order kinetic model because it has a high correlation coefficient ( $R^2 > 0.99$ ). Moreover, the theoretical value of  $q_e$  (3.14 mg g<sup>-1</sup>) is the closest to the experimental data (3 mg g<sup>-1</sup>). Hence, it can be concluded that the rate of direct adsorption controls the overall sorption kinetics. Additionally, according to Blanchard et al. [65], it can be assumed that the rate of the ion exchange reaction occurring on the surface between the adsorbent and adsorbate is responsible for the removal kinetics.

From the analysis of the intraparticle diffusion model, the value of  $C$  was found to be 0.63952 mg g<sup>-1</sup> which indicates that there is less contribution from intraparticle diffusion on the adsorption kinetics of methyl orange on the activated carbon. If the value of  $C$  is equal to zero, then it can be assumed that the

adsorption was solely governed by intraparticle diffusion. It is found that the plots of  $q_t$  versus  $t^{1/2}$  do not pass through the origin but intercept at the Y-axis which signifies that intraparticle diffusion as a rate limiting step is not only responsible but also some boundary layer effect as well.

## 4. Conclusions

In this study, activated carbon was successfully synthesized from a coconut shell with the potassium hydroxide activation process. This activated carbon was characterized by BET, XRD, FESEM and FTIR. A comprehensive study was performed on its adsorption efficiency for the removal of methyl orange from an aqueous solution.

BET surface analysis revealed that the synthesized sample is a mesoporous solid. XRD analysis proved that the sample had a perfect crystallite structure, and the FESEM images showed the presence of well-developed pores on the surface of the activated carbon sample.

A kinetic study showed that the adsorption behavior of the activated carbon followed the pseudo-second-order kinetic model. In addition, the experimental result showed that 100% dye removal was obtained by the adsorption process in 12 min.

## Conflict of Interest

No potential conflict of interest relevant to this article was reported.

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