Pretreatment Effect on CO Oxidation over Highly Ordered Mesoporous Silver Catalyst

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Highly ordered mesoporous silver material was successfully synthesized from a mesoporous silica template (KIT-6) with 3-D channel structure using the nano-replication method. The effects of H₂ or O₂ pretreatments on the catalytic performance of the mesoporous silver were investigated using a temperature programmed CO oxidation technique in a fixed bed reactor. The mesoporous silver material that was pretreated with H₂ exhibited an excellent catalytic activity compared to the as-prepared and O₂-pretreated catalysts. Moreover, this present mesoporous silver material showed good catalytic stability. For the CO oxidation, the apparent activation energy of the H₂-pretreated mesoporous silver catalyst was 61 ± 0.5 kJ mol⁻¹, which was also much lower than the as-prepared (132 ± 1.5 kJ mol⁻¹) and O₂-pretreated (124 ± 1.4 kJ mol⁻¹) catalysts.

Key Words: Nanostructure material, Mesoporous silver, Heterogeneous catalyst, CO oxidation, Pretreatment effect

Introduction

During the past few decades, considerable efforts have been devoted to the synthesis, modification and application of mesoporous materials because of their desirable physic-chemical properties such as high surface areas, well-ordered mesopores with regular pore sizes, and diverse framework compositions. After reports had been investigated on the synthesis of silica-based mesoporous materials, the research direction in these fields turned to the non-siliceous materials such as carbons, polymers, metal oxides, and metals.¹ Even though some non-siliceous mesoporous materials have successfully been produced using surfactants or polymers as the templates, the preparation of these mesoporous materials is still challenging. Recently, a nano-replication route, where mesoporous silica or carbon materials are utilized as a rigid template, is regarded as a promising method for producing nano-siliceous mesoporous materials.²

The catalytic oxidation of carbon monoxide (CO) is an important process in many applications such as air purification, pollution control devices, CO removal in heavy industry and vehicle exhaust, and fuel cells *etc.*³ In general, various types of metallic active species, such as Pd, ^{4,5} Pt, ^{6,7} Rh, ⁸ Au, ^{9,10} Cu, ¹¹ and Co, ¹² have been used for CO oxidation on the supports including TiO₂, Al₂O₃, SiO₂, CeO₂ and zeolite catalysts. Recently, a report showed that transition metal oxides such as Co₃O₄¹³ and CuO-Fe₂O₃ composites with mesoporous structures¹⁴ are active for CO oxidation at low temperatures. Tüysüz *et al.* reported that Co₃O₄ samples with high surface areas, were synthesized at different aging temperatures (40, 100 and 135 °C) and exhibited 100% CO conversion to CO₂ at low temperatures. ¹³ Cao *et al.* also reported that the mesoporous CuO-Fe₂O₃ composites with different CuO concentrations were synthesized using the surfactant-assisted method of nanoparticle assembly and exhibited excellent activity and stability with 100% CO conversion at 110 °C. Mesoporous RuO₂, which is replicated using cubic mesoporous silica, exhibits excellent activity with 100% CO conversion at 165 °C, ¹⁵ whereas mesoporous α -Fe₂O₃ had 100% CO conversion at 280 °C.¹⁴

Recently, highly ordered mesoporous silver material was synthesized using the nano-replication method with a cubic mesoporous silica template (KIT-6), and the surface hydrophobicity was controlled.¹⁶ Silver has attracted considerable attention because it can be applied in heterogeneous catalysis as well as advanced materials in the fields of antimicrobials and biosensors.^{17,18} Silver catalysts are also well-known for the epoxidation of ethylene.¹⁹ In this work, the catalytic properties of a mesoporous silver material were investigated for CO oxidation for the first time, and the pretreatment effects on the catalytic activity were addressed.

Experimental

Preparation of mesoporous silver samples. The mesoporous silica template, KIT-6, was synthesized following a method reported elsewhere.²⁰ A triblock copolymer (Pluronic P123, $EO_{20}PO_{70}EO_{20}$, Aldirch) and tetraethylorthosilicate (TEOS, Aldrich) were utilized as the structure-directing agent and the framework source, respectively. After calcination, the silica surface of KIT-6 was modified with methyl groups by refluxing a mixture containing 0.6 g hexamethyldisilazane (HMDS, 99%, Fluka), 150 mL of *n*-hexane and 3.0 g of calcined KIT-6 for 1 h.¹⁶ To synthesize the mesoporous silver, a solution (containing 1.18 g of AgNO₃ (99%, Aldrich), 0.9 g of EtOH and 0.9 g of distilled water) was impregnated into 3.0 g of the modified KIT-6

template using an incipient wetness method. After drying at 80 °C for 24 h, the composite was heated to 300 °C under a nitrogen flow for 24 h. Subsequently, the silica template was completely removed by treating the composite material with a 3 M NaOH solution three times at 0 °C. Finally, the mesoporous silver material was washed with distilled water and acetone several times and dried in a vacuum oven at room temperature for 12 h. The asprepared mesoporous silver material was pretreated with H₂ (or O₂) at 300 °C for 2 h with a flowing gas mixture containing 10% H₂ (or O₂) in Ar.

Material characterization and reaction measurements. The Xray diffraction patterns were obtained using the reflection mode of a Rigaku D/MAX-2200 ultima equipped with Cu K α at 30 kV and 40 mA. The scanning electron microscope (SEM) images were taken using LEO Supra 55 field emission scanning microscope that was operated at an accelerating voltage of 15 kV. The transmission electron microscope (TEM) images were obtained using a JEOL JEM 3010 at an accelerating voltage of 300 kV. The N₂ adsorption-desorption isotherms were collected on a Micromeritics Tristar system at a liquid N₂ temperature. CO was oxidized over the mesoporous silver catalyst at atmospheric pressure using a fixed bed reactor (inner diameter of 6 mm) from a temperature range of 25 to 300 °C, with a heating rate of 7.5 °C \min^{-1} . The feed gas (4% CO in O₂ and Ar) was introduced through a packed bed of catalyst pellets (20 - 40 mesh) at an hourly space velocity (GHSV) of 16,700 h⁻¹. The reaction gas mixture ratio of CO/O₂ was 1/5. The final reaction product was analyzed using a mass spectrometer (Pfeiffer-vacuum, QMS 200), and the CO conversion was defined as the number of moles of CO₂ produced after the reaction with respect to the amount of CO in feed gas.

Results and Discussion

Figure 1 shows the XRD patterns of the mesoporous silica template, KIT-6, and the mesoporous silver material obtained using the nano-replication method. KIT-6 exhibited the typical XRD peaks (Figure 1a) of a 3-D cubic (*Ia*3*d*) mesostructure.^{16,20,21} However, in the XRD pattern for mesoporous silver, a new peak appeared in the low angle region of Figure 1b, which corresponded to the position of the [110] reflection for *Ia*3*d* symmetry. The presence of the [110] reflection indicated that the cubic *Ia*3*d* mesostructures after the silica template was removed.¹⁶ The wide-angle XRD pattern (inset of Figure 1b) contained several peaks at $2\theta = 38.1^{\circ}$, 44.2° , 64.4° and 77.3° , which were characteristic of metallic silver.

The SEM and TEM images of the mesoporous silver material are provided in Figure 2. In Figure 2a, the mesoporous silver exhibited an irregular morphology, with sizes that were a few micrometers. The highly ordered mesostructures of the mesoporous silver were confirmed by the SEM (Figure 2b) and TEM (Figure 2c) images. In Figure 2d, the framework thickness of the mesoporous silver material was about 8 nm, which was very similar to the average silver domain size (about 8.2 nm) that was calculated from the XRD line-broadening using the Scherrer formula. This value was also similar to the pore size of the mesoporous silica template, KIT-6 (7.2 nm, Table 1).

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Figure 1. XRD patterns of (a) the silica template KIT-6 and (b) the mesoporous silver. The inset of (b) is a high-angle XRD pattern of the mesoporous silver.



Figure 2. (a,b) SEM images and (c,d) TEM images of the mesoporous silver material.

Figure 3 shows the N₂ adsorption-desorption isotherms and the corresponding BJH pore size distribution curves for the mesoporous silica template, KIT-6, and the mesoporous silver material. In Figure 3, all of the N₂ sorption isotherms were typical type-IV isotherms with hysteresis, indicating that the materials exhibited well-defined mesostructures. The physical properties of the mesoporous silica template and the corresponding mesoporous silver material are summarized in Table 1. The BET

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Table 1. Physical properties of the mesoporous silica template KIT-6 and the mesoporous silver materials.

Material	$S_{\rm BET} \left({{m^2}/{g}} \right)^a$	$D_{\rm pore} \left({\rm nm} \right)^b$	$V_{\rm tot} \left({\rm cc/g} \right)^c$
KIT-6	769	7.2	1.00
Mesoporous Ag	31	15.5	0.08

^aSurface areas calculated using the BET method. ^bMesopore diameters obtained from the N₂ adsorption branches using the BJH method. ^cTotal pore volumes estimated from the N₂ sorption isotherms at $p/p_0 = 0.99$.



Figure 3. N_2 adsorption-desorption isotherms of (a) the silica template KIT-6 and (b) the mesoporous silver material. The insets correspond to the BJH pore size distribution curves.

surface area of the mesoporous silver was 31 m² g⁻¹. The N₂ isotherm of the mesoporous silver had a well-defined step in the adsorption-desorption curves around a relative pressure, p/p_0 , of 0.8 - 0.9, and the corresponding BJH pore size obtained from the adsorption branch was about 15.5 nm, which was much larger than the wall thickness of the silica template probably because of the phase transformation from *Ia3d* to a *I4*₁/*a* (or lower) mesostructure for the mesoporous silver after the silica removal, as expected from the XRD patterns.

Figure 4 shows the dependence of the temperature programmed CO oxidation on the pretreatment conditions for the mesoporous silver materials, and the catalytic activities are listed in Table 2. Although the as-prepared mesoporous Ag exhibited the metallic phase in XRD pattern (Inset of Figure 1b), its surface might be partially oxidized. Therefore, the temperature programmed CO oxidation was performed without and with pretreatment using different atmospheres in order to investigate the effect of surface property on the catalytic activity. Without pretreatment, the CO oxidation started at 250 °C and reached a 100% conversion at 260 °C. In Figure 4a and Table 2, the H₂ pretreatment before the CO oxidation drastically improved the catalytic activity of the mesoporous silver material. The light-off temperature was much lower ($T_{\text{start}} = 65 \text{ }^{\circ}\text{C}$) than the as-prepared catalyst. The mesoporous silver material that was pretreated with O₂ exhibited a similar (or lower) catalytic activity to untreated mesoporous silver catalyst. The inset of Figure 4 shows an Arrhenius plot for the mesoporous silver catalysts that was obtained from the CO oxidation data, and the corresponding apparent activation energies (E_a) of the mesoporous silver cata-



Figure 4. Temperature-programmed CO oxidation dependence on the pretreatment conditions for the mesoporous silver material. The inset is an Arrhenius plot of CO conversion.

Table 2. Light-off temperature and activation energy of the CO oxidation for the mesoporous silver catalyst.

Pretreatment	Light-off temperature (°C)			E_{1} (la Lang 1^{-1}) ^d
	T_{start}^{a}	$T_{50}^{\ \ b}$	T_{100}^{c}	$E_{\rm a}$ (KJ mol)
as-prepared	250	258	260	132 ± 1.5
H ₂ treatment	65	161	195	61 ± 0.5
O ₂ treatment	225	251	267	124 ± 1.4

^aTemperatures when CO conversion starts. ^bTemperatures when CO conversion reaches to 50%. ^cTemperatures at CO conversion of 100%. ^dApparent activation energy calculated from Arrhenius plots.

lysts with various pretreatment conditions are listed in Table 2 for the CO oxidation. The activation energy of the H2-pretreated mesoporous silver $(61 \pm 0.5 \text{ kJ mol}^{-1})$ was much lower than the as-prepared and O₂-pretreated catalysts $(132 \pm 1.5 \text{ kJ mol}^{-1} \text{ and}$ 124 ± 1.4 kJ mol⁻¹, respectively) and slightly lower than the E_a of an Ag/CeO₂ catalyst (71 kJ mol⁻¹).²² Unlike Pt surfaces that facilitate CO to CO₂ through dissociative chemisorptions of oxygen and the molecular adsorption of CO, dissociative chemisorptions of oxygen and CO coverage do not easily occur on Ag metal surfaces.^{23,24} Bera *et al.* reported that the catalytic activity of 1 wt % Ag/CeO₂ ($T_{100} = 260$ °C) was higher than 1 wt % Ag/ Al₂O₃ ($T_{100} = 350$ °C) for CO oxidation.²² In this present study, similar results were observed for as-prepared mesoporous silver catalyst without any treatment, which exhibited a 100% CO conversion at 260 °C. However, the CO oxidation for the mesoporous silver material that was pretreated with H₂ began at a relati vely lower temperature and was complete at a temperature of 195 °C. According to these catalytic results, the surface species of the mesoporous silver material seems to be very important to the CO oxidation. Although all of the mesoporous silver materials exhibited metallic phases (Figure 5), the mesoporous silver material that was pretreated with H₂ might have sufficient defects for the dissociative chemisorptions of oxygen, and hence, an improved catalytic activity for the low temperature CO oxidation was shown, unlike the as-prepared and O2-pretreated meso-



Figure 5. XRD patterns of the mesoporous silver materials before and after the pretreatments.



Figure 6. Catalytic stability of the mesoporous silver material that was pretreated H_2 for the CO oxidation.

porous silver materials, which were less active for the CO oxidation.

Figure 6 illustrates the catalyst stability of the CO oxidation for the mesoporous silver material that was pretreated with H₂. Each CO oxidation was carried out from 25 to 300 °C. Even though the catalytic activity slightly decreased upon repeated CO oxidations, a significant deactivation was not observed in Figure 6.

Conclusions

A highly ordered mesoporous silver material was synthesized using the nano-replication method from a mesoporous silica template, KIT-6, with 3D cubic mesostructure (Ia3d), and the dependence of the CO oxidation on the pretreatment conditions was investigated for the material. The as-prepared and O₂-preJeong Kuk Shon et al.

treated mesoporous silver catalysts exhibited similar catalytic performances, showing a 100% CO conversion at 260 ~ 267 °C. However, the catalytic activity was dramatically improved by H₂ pretreatment, and the light-off temperature ($T_{\text{start}} = 65 \text{ °C}$) and activation energy ($61 \pm 0.5 \text{ kJ mol}^{-1}$) were much lower than the as-prepared and O₂-pretreated mesoporous silver catalysts ($T_{\text{start}} = 250 \text{ °C}$; $132 \pm 1.5 \text{ kJ mol}^{-1}$, and $T_{\text{start}} = 225 \text{ °C}$; $124 \pm 1.4 \text{ kJ mol}^{-1}$, respectively). The mesoporous silver material that was pretreated with H₂ also exhibited excellent catalyst stability, even though the catalytic activity and mesostructure slightly decreased upon repeating the CO oxidation cycle.

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