A Study on High Precision Temperature Control of an Oil Cooler for Machine Tools Using Hot-gas Bypass Method

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Abstract: This study aims at precise control of oil outlet temperature in the oil cooler system of machine tools for enhancement of working speed and processing accuracy. PID control logic is adopted to obtain desired oil outlet temperature of the oil cooler system with hot-gas bypass method. We showed that the gains of PID controller could be easily determined by using gain tuning methods to get the gain of PID controller without any mathematical model. We also investigated various gain tuning methods to design the gains of PID and compared each control performance for selecting the optimal tuning method on the hot gas bypass method through experiments. Moreover, we confirmed excellent control performance with proposed PI controller gain even though disturbances were abruptly added to the experimental system.

Key words: Oil Cooler, Hot-gas Bypass Method, PI Control, Electronic Expansion Valve, Gain Tuning

1. Introduction

Recently, working speed and processing accuracy are considered as very important factors for high productivity in the machine tools. Usually the high speed causes thermal displacement and structural deformation of the objects of machine tools.

An oil cooler is an inevitable device in the machine tools to prevent the thermal deformation. The oil cooler system makes a role to reduce the thermal load of the machining parts by controlling temperature of oil used on the machine tools.

Until now on-off control method[1] has been generally adopted in the oil cooler system. But it is difficult to control temperature precisely. Also, electrical power consumption is increased because of frequent switching operation in a compressor of the oil cooler system.

Variable speed control of a compressor[2] and hot-gas bypass method[3~6] were developed to solve these problems. The variable speed control of a compressor with an inverter enables precise temperature control and can reduce electrical power consumption. However, this control method needs extra device like an inverter. Therefore, it costs highly and makes structure of the oil cooler system complicated. On the other hand, the hot-gas bypass method is simple in structure and possible to control temperature comparatively precisely. For that reason, we focused on the hot-gas bypass method in this paper.

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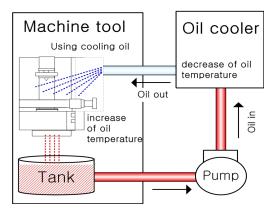


Figure 1: Schematic diagram of an oil cooler systems

Conventional researches about hot-gas bypass method were mainly focused on the evaluation of performances of a controller. However, they did not deal with abrupt disturbances added on machine tools. Moreover, design methodology of the controller was not investigated in detail.

In this paper, we will show the design process by the PID controller in order to obtain desired oil outlet temperature of the oil cooler. Opening angle of electronic expansion valve(EEV), hot-gas bypass valve, is considered as a control variable in this scheme.

It is important to determine gains of the PID controller appropriately satisfying control objective. In general, the gains are obtained on the basis of mathematical model. However, it is very difficult to get a practical dynamics of the controlled system. Accordingly, gain tuning method is used in this paper.

The validity of designed controller based on the gain tuning method is verified through the experiment. Moreover, we confirmed excellent control performance with proposed PI controller when disturbances were abruptly added to the experimental system.

Control of an oil cooler with hot-gas bypass method

2.1 Oil cooler system with hot-gas bypass

The oil cooler system is used to control the oil temperature of machine tools as a kind of refrigerators. Low temperature oil cooled by the oil cooler system is supplied to the machining parts to reduce the thermal load.

Figure 1 shows a schematic diagram of an oil cooler type. The oil with high temperature caused by absorbing thermal load gets back to a tank and then moves to an oil cooler through a pump. Consequently, oil outlet temperature of an oil cooler is retained as constant value to prevent thermal deformation.

There are three types in hot-gas bypass methods. The first type is that the which refrigerant comes from the compressor's exit is sent to the evaporator's entrance. The second type is that the refrigerant which comes from the compressor's exit is sent to the evaporator's exit. The third type is that the refrigerant which comes from the compressor's exit and the condenser's exit is mixed together and then is sent to the evaporator's exit.

In the first method, the refrigerant in the compressor's exit is in a low temperature state. Therefore, it can operate an oil cooler safely. Also, it is very easy to change cooling capacity. So, we aimed at the design of control system by this method[3].

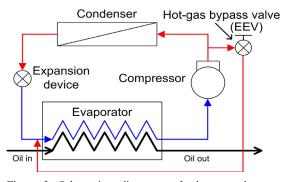


Figure 2: Schematic diagram of hot-gas bypass systems

Table	1:	Specifications	of	EEV	
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Operating range	0~500 [pulse]		
Rated voltage	DC 12 (V)		
Max working pressure	3.3 [Mpa]		

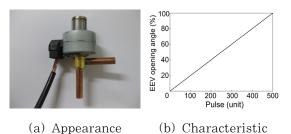


Figure 3: Appearance and characteristic of EEV

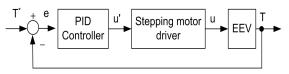


Figure 4: Block diagram for EEV control

Figure 2 shows schematic diagram of hot-gas bypass. The refrigerant which comes from the compressor's exit is in high-temperature and high-pressure. It is detoured to the evaporator's entrance, and it is mixed with the low-temperature and low-pressure refrigerant. It has brought that the evaporator's temperature is increased and the cooling capacity is decreased. Therefore oil outlet temperature of an oil cooler can be retained constantly by controlling opening angle of EEV appropriately.

Table 1 indicates the main specification of the EEV. Figure 3 (a), (b) appears the appearance of EEV and variation of EEV opening angle by the pulse input respectively.

2.2 Design of a PID controller

Figure 4 is a block diagram of a PID control system for controlling the oil outlet temperature of an oil cooler.

The temperature error is sought by using an equation of $e = T^* - T$, and the PID controller generates control input so that it becomes 0.

Manipulated variable u(t) is decided by the PID controller proportional – integral – derivative shown in the equation (1).

$$u(t) = K_p e(t) + K_i \int e(t) dt + K_d \frac{d}{dt} e(t)$$
(1)

Designing a PID controller is decided by the PID controller shown in the equation (1). PID controller is to decide the gains K_p, K_i, K_d in order to establish control purpose.

The oil cooler is composed of a compressor, an expansion device and heat exchangers. Moreover, the components are deeply connected with pipes and valves each other. Hence. they show inherent nonlinear characteristics in operational ranges. Accordingly. it is almost impossible to identify dvnamic exact characteristics and to get a practical

mathematical model of the oil cooler system. In this paper, we investigate gain tuning methods to obtain the gains of PID controller and compare each control performance for selecting the optimal tuning method on the hot gas bypass method through experiments.

Table 2: Specification of the test unit

Compressor	Rotary type, 1HP		
Condenser	Air-cooled fin and tube type		
Evaporator	Plate heat type exchanger		
Refrigerant	R-22		

Table 3: Experimental conditions

Oil flow rate	25 [l/min]		
Air temperature	35 (°C)		
Sampling time	1 [sec]		

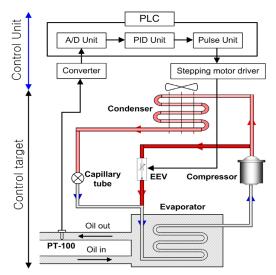


Figure 5: Control system of an oil cooler for a machine tool

3. Experiments

The oil cooler system usually is consisted of four components : a compressor, a condenser, an evaporator and an expansion valve.

Figure 5 shows control system of an oil

cooler for the machine tool and configuration of experimental equipments is shown in Figure 6. It is noted here that the bold line represents hot-gas bypass path in Figure 5.

The control parts of the oil cooler system is composed of a PLC (Programmable Logic Controller) and a stepping motor driver. Also, the PT-100, a temperature sensor, and a temperature/voltage converter are used for temperature detection and signal conversion.

The oil outlet temperature measured by the PT-100 is converted to voltage by a converter and it is transmitted to the PLC. The detected oil outlet temperature and the set value of temperature are compared with each other in the PLC, and then control error is calculated. The manipulated variable is decided so that the error becomes 0 in the PID controller. It is sent to a stepping motor driver. The stepping motor driver controls opening angle of EEV.

In order to monitor the operating situation of the oil cooler, temperatures of main parts are measured by using a T-type thermocouple. The various information such as temperature, electric power, valve's opening angle, oil flow rate, etc. collected to a data acquisition device, and also transmitted to a PC to record the data.

The oil cooler is designed to have cooling capacity of 3.51kW under the room temperature of 35°C and to keep the oil outlet temperature of 35°C. The thermal load of the experimental system is added by an electrical heater instead of a machine tool. Table 2 represents specification of the test unit and table 3 indicates experimental conditions.

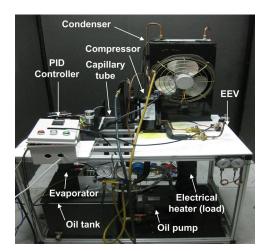


Figure 6: Experimental equipments

4. Results and Discussions

The set point of oil outlet temperature is fixed at 35°C considering characteristics of machine tools. The value is supposed as constant value during operation in this paper. The design objective is to maintain the oil outlet temperature within an allowable error even if disturbances are added to the system. The steady-state characteristics are considered more important than the transient characteristics in this system.

4.1 Gain tuning method of PID controller

At first, we have to determine the gains of PID controller through experimental method because it is difficult to get a practical mathematical model. The method of step response, critical oscillation and relay auto tuning are well known as t aical gain tuning method.

Figure 7, Figure 8, Figure 9 indicate experimental results of a step response, critical oscillation response and relay auto tuning response respectively. From the Figure 7. we know that step response method are not available for tuning of PID controller. The gains of PID controller obtained from Figure 8. Figure 9 appear in Table 4.

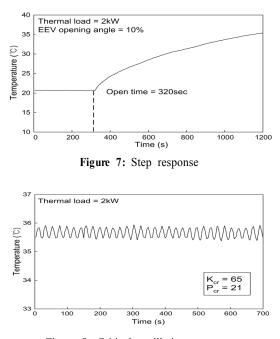


Figure 8: Critical oscillation response

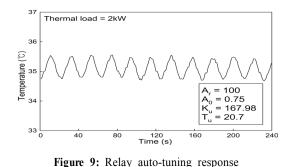


Table 4: PID gain according to tuning method

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Tuning method	Controller	Kp	Ki	K_d				
Critical oscillation	PI	29.3	1.67	0				
Critical oscillation	PID	39.0	3.71	102				
Relay auto-tuning	PID	84.9	13.8	131				

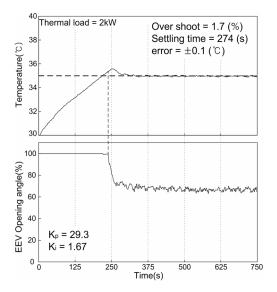


Figure 10: PI control response by critical oscillation

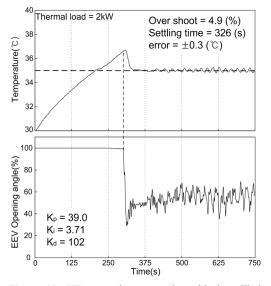


Figure 11: PID control response by critical oscillation

Figure 10, Figure 11 show control performance of PI and PID by the critical oscillation response when we set the thermal load as 2kW respectively. We know that the overshoot and error of PI control is smaller than the one of PID control.

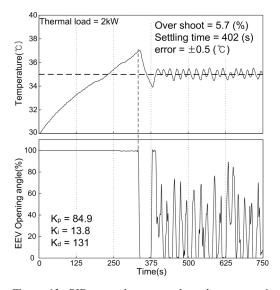


Figure 12: PID control response by relay auto-tuning

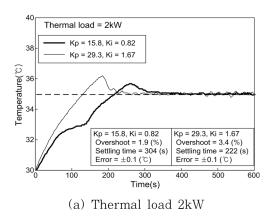
Figure 12 appears PID control performance by relay auto tuning response. From these results. PI control gains bv critical oscillation method show much better performance than examined other methods. Therefore we adopt the critical oscillation method for gain tuning.

4.2 Evaluation of control performance according to variation of load

The control performances obtained from different thermal load conditions were compared with each other.

Figure 13 (a), (b) show PI control results when we set a thermal load as 2kW and 3kW respectively. As a result, the gains of PI controller at the thermal load 3kW are $K_P = 15.8, K_I = 0.82$ (case I). The gains of PI controller at the thermal load 2kW are $K_P = 29.3, K_I = 1.67$ (case II). As shown in results, the overshoot of case II is larger approximately 1.5% than that of case I. The settling time of case II is faster about 80sec than that of case I. Also, the steady-state errors of caseII was the largest as ± 0.3 °C, compared with ± 0.1 °C for case I.

Figure 14 (a), (b) show control responses when disturbances were abruptly added to the experimental system. We compare control performance with PI controller of case I and that of case II when the thermal load changed from 1kW to 3kW respectively. The steady-state error of case I was maintained within \pm 0.2°C as allowable design specification. Also it is controlled well without vibration phenomenon of the EEV to change opening angles in case I. From the results, we know that case I is better than case II.



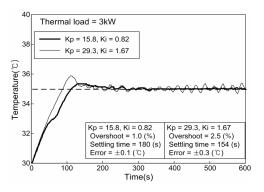




Figure 13: Results of control performance with PI controller

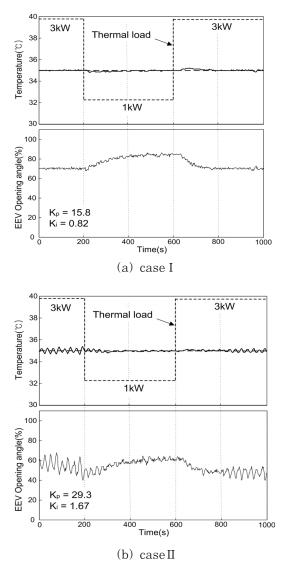


Figure 14: PI control response by critical oscillation under abruptly added disturbance

5. Conclusions

PI controller of the oil cooler with hot-gas bypass method was designed in order to maintain oil outlet temperature as a constant set value.

The gains of PI controller were easily decided by the critical oscillation gain tuning method. Through experimental results, oil outlet temperature could be controlled well within allowable design specification of ± 0.2 °C error range. Moreover, the PID controller designed by the critical oscillation method showed excellent control performance even though disturbances were added to the experimental system instantaneously.

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