⊙ 硏究論文

An Experimental Study of the Swirling Flow and Heat Ttransfer Downstream of an Abrupt Expansion in a Circular Pipe with Uniform Heat Flux

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선회류를 동반한 급확대 원관내에서의 열전달 특성에 관한 실험적 연구

권 기 린 · 장 태 현

Key words : Turbulent flow(난류유동), Heat transfer(열전달), Swirling flow(선회유동), Abrupt pipe expansion(급확대관), Swirl chamber(와류실), Swirl generator(스월발생기)

요 약

실험 데이터는 급확대비 3 : 1 팽창의 시험관에서의 실험결과를 나타내고 있으며, 실험에 이용된 동작유체로써는 공기가 사용되었다. 입구관에서 레이놀즈수는 60,000으로부터 120,000까지 변하게 하였고, 스월강도는 0으로부터 16까지 변화되게 하였다. 균일한 열 플럭스 경계조건이 사용되었는데, 그 결과 관벽온도 및 체적온도는 24℃로 부터 71℃까지에 걸쳐 나타났다. 플롯상에 국소 Nusselt수는 최대 열전달점에서 정점을 이루는 모습을 보여 주고 있다. 스월강도가 0으로부터 최대값으로 증가 되었을때, 최고 Nusselt수의 위치는 시험관에서 4로부터 1스텝 하이트로 변경되는것이 조사되었다. 이러한 최대 Nusselt수의 상류부 이동은 완전 발달된 유동에서의 값보다 2.2배에서 8.8배나 많은 그의 크기를 증가시킨다고 할수 있다.

Nomenclature

d : upstream tube diameter
D : downstream tube diameter
f : friction factor
k : thermal conductivity of air
L : distance along the plenum chamber
$\dot{m}$: mass flow rate
Tb : bulk temperature
Nu_{DB} : fully developed Nusselt number for turbulent pipe flow represented by Dittus – Boelter corelation
Pv : velocity pressure
Tw : wall temperature

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R : radius of a downstream tube
Re : Reynolds number in upstream tube
u : local velocity
$\bar{u}$: mean axial velocity in upstream tube
x : axial distance from expansion face
y : distance from the wall
ρ : local density at the point of interest

1. Introduction

Experimental research on the heat transfer in regions of seperated and reattached flows inside of pipes and ducts goes back at least to the work of Boetler et al., in 1948.

Boetler et al. reported maximum heat transfer coefficients near the point of reattachment about four times the fully developed flow values.

Without swirl, flow through a sudden expansion produces mixing rates and subsequently heat transfer coefficients which are substantially higher downstream of the expansion than those which would be obtained at the same Reynolds number in the entrance region of pipe[1-4].

Swirl is also responsible for increased shear rates, greater turbulence production, and longer path lengths for a particular fluid particle so that the effect of swirl like the effect of the sudden expansion, is also to increase heat transfer rates significantly over those found in purely axial pipe flow[5-8].

Recently, Dellenback et al.(1987) reported an ambitious investigation of the flowfield and related heat transfer behavior for the present problem, incluiding swirl[9-11].

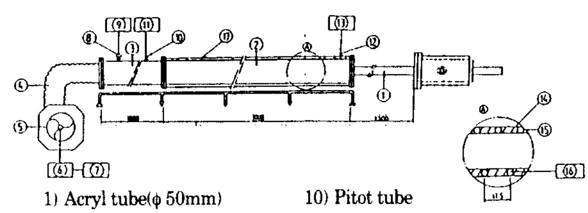
However, many studies of heat transfer of the swirling flow or unswirled flow in a abrupt pipe expansion are widely carried out, the mechanism is not fully found evidently due to the instabilities of flow in a sudden change of the shape, appearance of turbulent shear layers in a recirculation region and secondary vortex near the corner. The purpose of this study is to obtain new accurate data throughout an experimental study of the swirling flow and heat transfer downstream of an abrupt expansion in a circular pipe with uniform heat flux.

2. Experimental Apparatus and Pro-cedure

The entire experimental apparatus is shown schematically in Fig.1.

An experimental test - rig was manufactured to permit a detailed interrogation of all flow variables. The rig incorporated a specially designed swirl generator, fitted to the inlet of a perspex circular pipe, enabling varying intensities of swirl flow to be stimulated over the Reynolds number range of 60 - 120 $\times$ 10^3(in the upstream tube).

An identical pipe, manufactured out of copper, enabled a constant heat flux to be applied at its outer surface, thereby permitting a corresponding investigation of the heat transfer phenomena.



1) Acryl tube(ϕ 50mm)
2) Copper or Acryl tube(ϕ 150 mm)
3) Steel pipe(ϕ 150mm)
4) Flexible connector
5) Turbo fan(220 $\times$ 10HP)
6) Motor(220 $\times$ 10HP)
7) R. P. M. regulator
8) Multi pitot tube(Tobar 301)
9) Inclined manometer
10) Pitot tube
11) Electronic manometer
12) Thermocouple(k type)
13) Electronic thermometer
14) Insulation
15) Heating coil(ϕ 4mm, space 17.5mm)
16) Voltage regulator
17) Measurement hole(ϕ 2.5mm)

Fig. 1 Schematic diagram of experimental apparatus

2 - 1. Pressure and velocity measurement

The acrylic test section used for the velocity and pressure measurements is a plexiglass cylinder of internal diameter 150mm and thickness of 5mm, lenght of 3,000mm.

If x denotes the axial distance along the test section and d denotes the internal diameter of the test pipe then x/d locates a station measurement position in non - dimesnional form on the test section. The inlet is located at $x/d = 0$ and the outlet located at $x/d = 60$.

The unheated upstream tube(inside diameter 50mm) and the expansion face were the same plexiglass components used in the flowfield measurements.

The swirl generator is located upstream of the test section and is composed of a plenum chamber and a swirl generator. The plenum chamber is a plexiglass cylinder of outer diameter 200mm and thickness of 5mm, length of 1,500 mm. The plenum chamber is attached to the test section by wooden flanges and the generator.

The section of the swirl generator is shown on Fig. 2. To create swirl, a swirl generator is

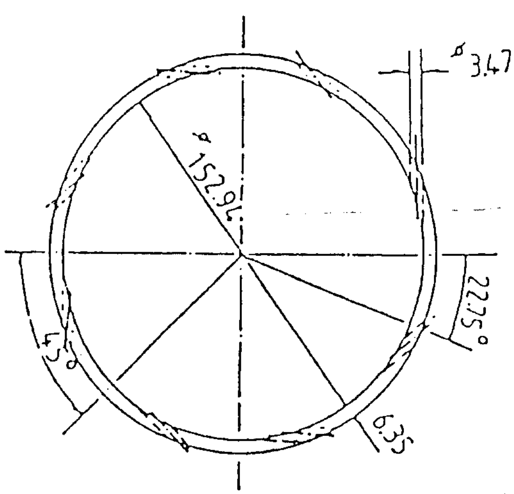


Fig. 2 A cross section of the swirl generator
(All dimensions are in mm)

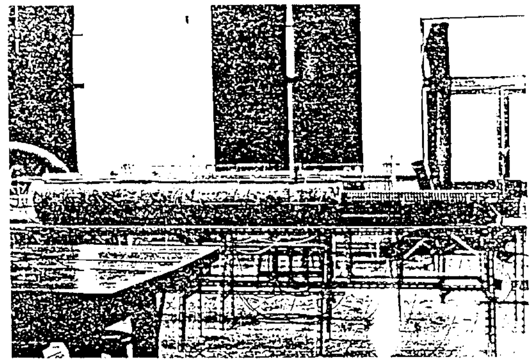


Fig. 3 Photograph of the test tube mounted with heating coil

placed within the plenum chamber. The generator consists of a 165.5mm outside diameter plexiglass cylinder with a 6mm wall thickness and 240mm length.

The design of the generator refers to Chaboki[12] to the effect that it produces a near perfect axisymmetric swirl.

The pressure distrubution along the length of the test section is obtained by a series of pressure tappings located on the test pipe connected to a multimanometer by plastic tube.

The blower is located downstream of the test section which produces the air suction. For friction factor measurement an identical apparatus is used and the pressure gradients are obtained along the length of the test section and substituted into the friction factor relation described later.

The static pressure signals were then conveyed to the multimanometer by plastic tube. Air is drawn through the generator and through the tangentially cut holes, resulting in the generator of swirl.

2 - 2. Fluid Flow Measurement

The torbar 301 pressure gauge is also located between the test section outlet and the blower. The torbar 301 gauge enables the correct Reynolds number flow to be ascertained by connecting to and inclined manometer and obtaining the pressure difference in mm WG required for a particular Reynolds number flow. The flow is adjusted by a control valve located on the blower. The flow rate was measured downstream of the test section by a self averaging pitot tube, the torbar 301. A honeycomb mesh was used to control the flow characteristic at the inlet of the impact tube.

These flow - measuring devices were connected to a micromanometer capable of measuring pressure differences via tygon tubing.

2 - 3. Temperature Measurement

The copper heat transfer test section was of the same dimensions as the acrylic test section used for the velocity and pressure measurements.

The copper electrodes were connected to a variable transformer in series with a 240V AC regulator, which allowed an adjustable, and stable AC voltage to be dialed into the electrodes.

Voltages used in the experiments ranged 240V AC, providing a total power to the heated tube of 1,750W.

This resulted in heat fluxes of 0.011W/cm^2.

The local tube wall temperatures were measured with thermocouples(0.08mm C - A) epoxied to the back side of the Intrex through small holes in the tube wall. There were 15 calibrated thermocouples located at different axial positions along the tube. Also, measurement of the radial temperature fields could then be accomplished by installing the probe in the traversing mechanism.

2 - 4. Data reduction

The Standard formula for calculating velocity from velocity pressure is u

$$u = 1.291\sqrt{Pv} \qquad (1)$$

The measured pressure distributions were used to evaluate local apparent friction factors.

The friction factor was obtained by local application of its equation of definition

$$f = (-dp/dx)\mathrm{D}/1/2\rho\bar{u}^2 \qquad (2)$$

Heat transfer tests were performed in a horizontal copper tube by passing AC current in the tube wall.

Local heat transfer coefficients were evaluated from the basic definition

$$dq = \dot{m}\,Cp\,dTb \qquad (3)$$

$$h = \frac{\dot{m}CpdTb}{2\pi dx(Tw - Tb)_{mean}} \qquad (4)$$

The local heat flux is designated by q, the local wall temperature by Tw and the local bulk temperature by Tb.

A dimensionless representation was made in terms of the local Nusselt number

$$Nu = \frac{h\mathrm{D}}{k} \qquad (5)$$

Here, D is the downstream tube diameter, k is the thermal conductivity of air at thelocal bulk temperature.

The local convective heat flux q was determined by correcting the electric power input for axial conduction in the tube wall and for losses through the insulation that surrounds the test section. The value of Tb at any axial station x was found from an energy balance on the fluid, using a control volume which extended from x=0 to x=x and integrating the aforementioned local q values to obtain the heat input to the control volume. Values of the local wall temperature Tw were available from the experimental data.

3. Results and Discusson

3-1. Axial velocity distributions

Fig.4 shows the axial velocity variation with radial distance along the pipe for no swirl flow and Re=120,000. For Re=120,000, it can be seen that the axial velocity distribution rise from tube wall to tube centre and as y/R>0.4 rises rapidly. At x/d=1 the flow pattern apprximates to that at X/H=1 by Habib and McEligot[9].

In particular, negative values occured due to the reversed flow near the wall at x/d=1,2,4.

Fig. 5 shows the axial velocity variation with

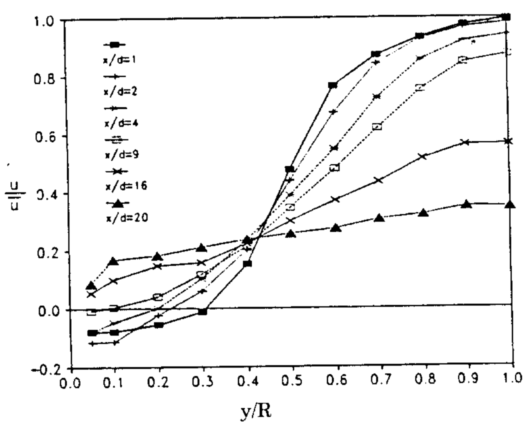


Fig. 4 Axial velocity profiles for Re=120000 with a concentric expansion

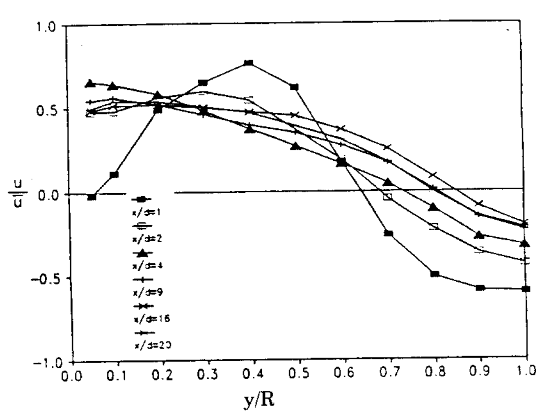


Fig. 5 Axial velocity profiles for Re=80000 with swirling flow at L/d=8

radial distance along the pipe for swirl flow and Re=80,000 at L/d=8. At L/d=8 the flow pattern resembles that at S=0.60 by Dellenback[11]. It can be seen that with increasing axial distance the highest axial velocities move toward the tube wall. As the swirl increase, the reattachment point of the separated region in the corner moves sucessively closer to the entrance and the central jet spreads more rapidly towards the wall. These features are also demonstrated by Sultanian[10].

3-2. Friction factor

Fig.6 shows the friction factor distributions with axial distance along the pipe as Reynolds number varies from 60,000 to 120,000, swirling flow at L/d=8, heat flow=1.75kW.

For all Reynolds number, friction factor of the test tube decreased rapidly at x/d=4 regardless of the inlet flow boundary condition in swirled flow.

The value of friction factor showed a slight increase in the entrance region of pipe when the Reynolds number was larger than any other Reynolds numbers, as shown in Fig. 6. It shows a gradient increase up to x/d=4 but a sharp decrease between x/d=4 and x/d=15,

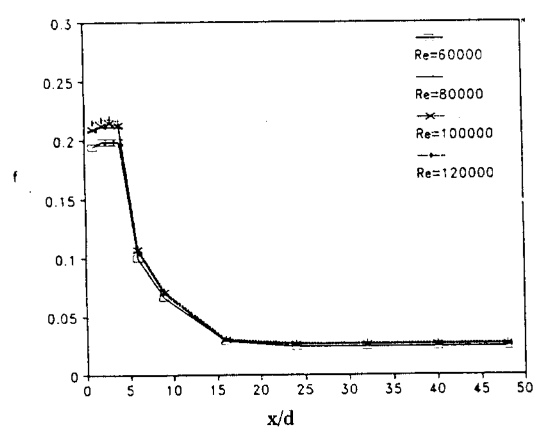


Fig. 6 Friction factor distribution for various Reynolds numbers with swirling flow at L/d=8, heat flow=1.75kw

showing a constant consistency.

3 - 3. Temperature distributions

Fig.7 - 1 and 8 - 1 show the wall and fluid bulk temperature variation with for unswirled flow as Reynolds number varies from 80,000 to 120,000. For all Reynolds number, the wall temperature showed a curve of parabolic variation at $16 \leq x/d \leq 48$. The bulk temperature showed a minimum value at $x/d = 6 \sim 9$, but it showed a linear distribution of increase. In addition, the values of *Tw*, *Tb* showed a greater increase at Re = 80,000 than any other Reynolds numbers.

Fig.7 - 2 and Fig.8 - 2 show the wall and fluid bulk temperature variation with axial distance along the pipe for swirling flow. It shows that the wall temperature initially rises rapidly, then reduces, until the distribution of *Tw* becomes linear with axial distance, whereas the fluid bulk temperature exhibits a linear increase with axial position virtually from the pipe inlet.

The temperature distributions give some qualitative suggestions concerning the phenomenon being studied,ie., heat transfer effectiveness downstream of an abrupt expansion.

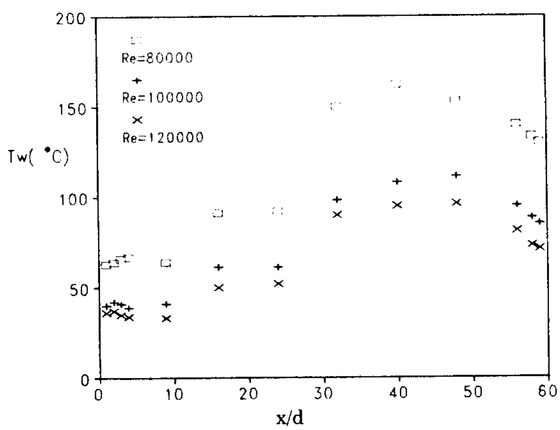


Fig. 7 - 1 Distribution of wall temperature along the test tube with the abrupt expansion

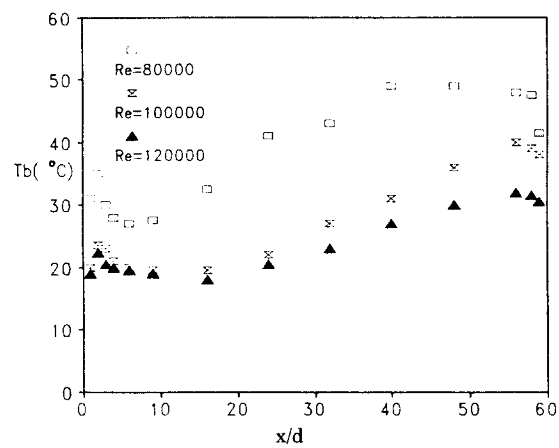


Fig. 8 - 1 Distribution of bulk temperature along the test tube with the abrupt expansion

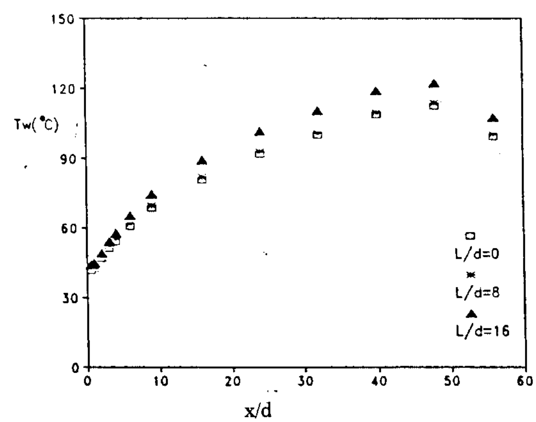


Fig. 7 - 2 Distribution of wall temperature along the expansion for Re = 60000 with swirl

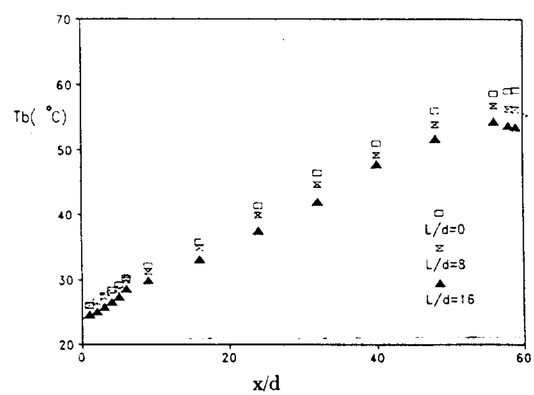


Fig. 8 - 2 Distribution of bulk temperature along the test tube expansion for Re = 60000 with swirl

Nusselt number is inversely proportional to the wall - to - bulk temperature difference for a fixed heat flux and constant properties.

And, the value *of Tw* showed a greater increase at L/d=16 than any other L/d ratios.

For all Reynolds number, the value of *Tb* showed a minimum value at the pipe inlet, it also exhibited a linear increase with axial distance along the pipe. The value of *Tb* showed a greater increase at L/d=0 than any other L/d ratios. It is seen that an effect of swirl is to increase the *Tb*.

3 - 4. Nusselt Number variations

Fig. 9 - 1 presents the measured axial variations in normalized Nusselt number as a function of swirl strength for nominal Reynolds of 60,000. The peak Nusselt numbers increase consistently in magnitude and move upsteam with increasing swirl strength.

This upstream migration of Nu_m is a direct result of the shortening reattachment length. The shortening of the recirculation region causes shear rates and hence production of turbulence kinetic energy to increase with consequently higher heat transfer rates.

The Nu/Nu_{DB} ratio showed a greater increase at L/d=0 than any other L/d ratios.

Fig. 9 - 2 presents the measured axial variations in normalized Nusselt number as a function of swirl strength for nominal Reynolds of 80,000.

The Nu/Nu_{DB} ratio also showed a geater increase at L/d=0 than any other L/d ratios. These features are also demonstrated by Dellenback[11]. In Figs 9 - 1 and 9 - 2, the Peak Nu/Nu_{DB} occurred at 1 step height and it showed a greater increase at Re=60,000 than at Re=80,000.

In addition, comparison of the unswirled flow result from Figs. 9 - 1 and 9 - 2 demonstrates

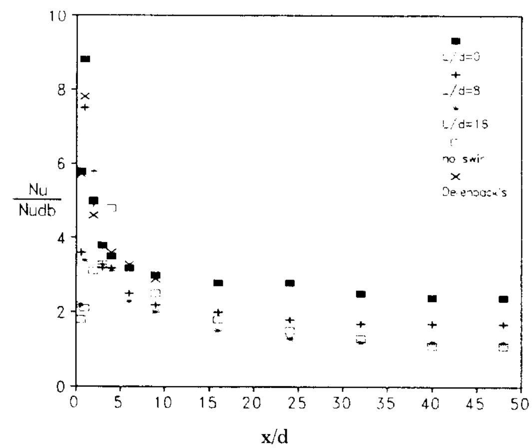


Fig. 9 - 1 Distribution of Nu/Nudb along the test tube abrupt expansion for Re=60000 with swirl

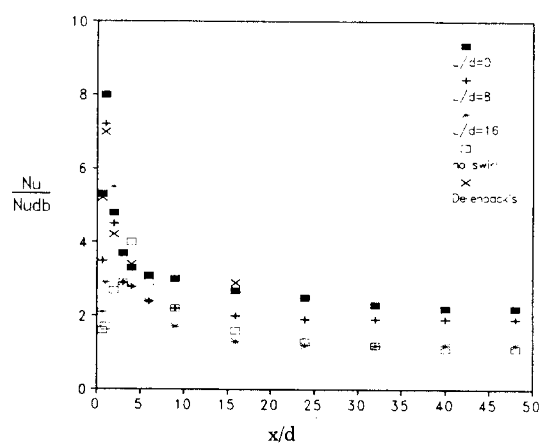


Fig. 9 - 2 Distribution of Nu/Nudb along the test tube abrupt expansion for Re=80000 with swirl

that larger enhancements in heat transfer rates over straight pipe flow occur at lower Reynolds numbers. This feature is simply rationalized by the observation that convection heat trasfer behavior in separated flow is commonly found to depend on $Re^{2/3}$.

4. Conclusions

Experiments were carried out for the turbulent swirling flow and heat transfer downstream of an abrupt circular pipe expansion.

The uniform heat flux condition was imposed to the downstream of the abrupt expansion by using an electrically heated pipe. The following conclusions are drawn from the test data.

1. The location of the peak Nu/Nu_{DB} showed at the point of 1 step height for Re=60,000, 80, 000 in the swirling flow abrupt concentric expansion, whereas it showed at the point of 4 step heights for same Reynolds number in unswirling flow expansion.

2. Axial velocity increased rapidly at r/R=0.4 in the abrupt concentric expansion turbulent flow through the test tube in unswirled flow, whereas it showed that with increasing axial distance the highest axial velocities move toward the tube wall in the case of the swirling flow abrupt expansion.

3. Friction factor of the test tube showed a gradient increase up to x/d=4 but a sharp decrease between x/d=4 and x/d=15, showing a constant consistency.

4. The wall temperature and bulk temperature showed a minimum value at the pipe inlet, and the bulk temperature also exhibited a linear increase with axial distance along the pipe but the wall temperature initially rises rapidly.

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